

## **A Numerical Solution of Three-Dimensional Unsteady State Heat Equation**

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**Abstract.** Heat equation is a partial differential equation that describes the distribution of temperature (heat) in a given body over time. In this study, a finite volume based method is used to solve three-dimensional heat equation. A MATLAB code is developed to implement the numerical method in a unit cube. The stability of the numerical scheme is analysed using the Von Neumann method. An example is provided in order to demonstrate the method. The numerical solution by the method is in an excellent agreement with the exact solution for the example considered. The computational procedures used in this study can provide good insights to solve a three dimensional diffusion equation arising in many physical phenomena.

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**Keywords:** Heat equation; Unsteady; Three-dimensional; Finite volume method; MATLAB code.

### **Index to information contained in this paper**

1. Introduction
2. Finite volume discretization
3. Stability analysis
4. A test problem and solutions
5. Conclusion

## **1. Introduction**

If parts of a body are exposed to different temperature conditions, heat flows through the body from the region of high temperature to that of lower temperature [15]. Temperature distribution includes in a metal block or wire, in a liquid, in a room, in a living tissue and many others. The temporal and spatial temperature distribution in the body is described mathematically by heat equation. In order to understand the temperature distribution, a solution of heat equation is required. Analytical and numerical methods are employed to solve heat equation [13]. Finite difference, finite element and finite volume methods have been used to obtain numerical the solutions for one or two dimension [2, 5, 12, 14, 17, 18].

Numerous numerical solutions of three-dimensional heat equation have been reported in literature. Sutradhar et al. [16] applied Laplace transform boundary element method to solve the transient heat the equation by performing the numerical implementation using a Galerkin approximation. Patil et al. [11] presented an algorithm to solve three dimensional steady state heat transfers in cube using finite volume grid technique. The computation was performed with MS excel. Ang and Gumel [1] used a boundary integral method together with finite difference method to solve three-dimensional heat equation. Gavete et al. [4] solved the three-dimensional elliptic and parabolic equations using generalized finite difference method. In solving partial differential equations (including heat equation) effective computer program and precise implementation of boundary conditions are required.

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## 2. Finite volume discretization

The three-dimensional heat equation is represented as [8]:

$$\frac{\partial u}{\partial t} = \alpha \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) \quad (1)$$

where  $u(x, y, z, t)$  is temperature and the constant  $\alpha$  is thermal diffusivity. Using del operator and taking  $\alpha$  to be 1 [6], (1) can be written as

$$\frac{\partial u}{\partial t} = \nabla \cdot (\nabla u) \quad (2)$$

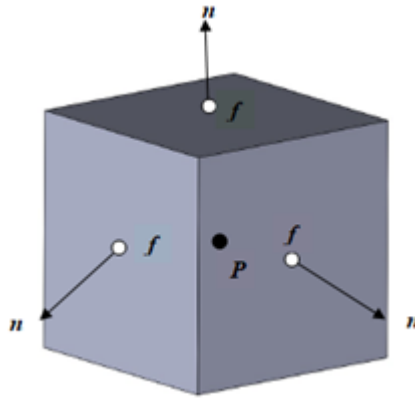


Figure 1. 3D control volume.

Integrating (2) over the control volume  $\Omega$  (see Figure 1), we get

$$\iiint_{\Omega} \frac{\partial u}{\partial t} d\Omega = \iiint_{\Omega} \nabla \cdot (\nabla u) d\Omega \quad (3)$$

The integral in the left side of (3) is evaluated as [10]

$$\iiint_{\Omega} \frac{\partial u}{\partial t} d\Omega = \frac{\partial u}{\partial t} \Delta V \quad (4)$$

where  $\Delta V$  is the volume of the control volume.

Applying Gauss's Divergence Theorem in the left right side of (3) we have

$$\iiint_{\Omega} \nabla \cdot (\nabla u) d\Omega = \iint_S (\nabla u) \cdot \mathbf{n} dS \quad (5)$$

where  $S$  is the boundary surface of the control volume and  $\mathbf{n}$  is the outward unit normal to  $S$ .

$$\iint_S (\nabla u) \cdot \mathbf{n} dS = \sum_f \left( \iint_S (\nabla u)_f \cdot \mathbf{n}_f dS \right) \approx \sum_f (\overline{\nabla u})_f \cdot \mathbf{n}_f A_f \approx \sum_f (\nabla u)_f \cdot \mathbf{n}_f A_f \quad (6)$$

where  $f$  indicates summation over face of each control volume,  $(\overline{\nabla u})_f$  is the average

temperature gradient at the face  $f$ ,  $(\nabla u)_f$  is the temperature gradient at the center of the face  $f$ ,  $\mathbf{n}_f$  is the outward unit normal to the  $f$  and  $A_f$  is the area of the face  $f$  [9].

From (3), (4) and (6), we get

$$\frac{\partial u}{\partial t} \Delta V = \sum_f (\nabla u)_f \cdot \mathbf{n}_f A_f \tag{7}$$

In order to illustrate the finite volume solution procedure to three-dimensional heat equation, let us consider unsteady heat flow in a unit cube shown in Figure 2.

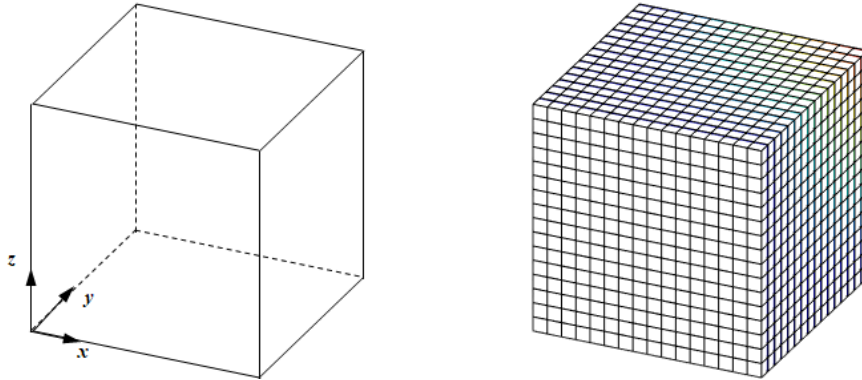


Figure 2. Geometry and finite volume mesh of heat flow domain.

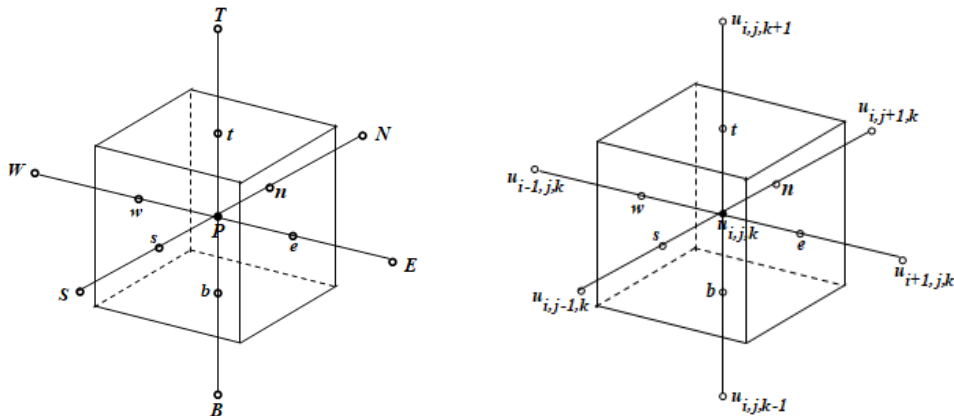


Figure 3. Face and center values at a control volume.

If we apply (7) on a control volume (Figure 3), we get

$$\frac{\partial u}{\partial t} \Delta x \Delta y \Delta z = \left[ \left( \frac{\partial u}{\partial x} \right)_e - \left( \frac{\partial u}{\partial x} \right)_w \right] \Delta y \Delta z + \left[ \left( \frac{\partial u}{\partial y} \right)_n - \left( \frac{\partial u}{\partial y} \right)_s \right] \Delta x \Delta z + \left[ \left( \frac{\partial u}{\partial z} \right)_t - \left( \frac{\partial u}{\partial z} \right)_b \right] \Delta x \Delta y \tag{8}$$

Here the expressions in the brackets with  $e$ ,  $w$ ,  $n$ ,  $s$ ,  $t$  and  $b$  represent the values of the expressions at the center of east, west, north, south, top and bottom faces of the control volume respectively and  $\Delta x$ ,  $\Delta y$  and  $\Delta z$  are the grid spacing in  $x$ ,  $y$  and  $z$  directions. The symbols  $P$ ,  $E$ ,  $W$ ,  $N$ ,  $S$ ,  $T$  and  $B$  in Figure 3 indicate center of the control volumes at which the values of temperature field are computed. Approximating the time derivative using

forward difference and spatial derivatives using central difference [10] in (8), for interior control volumes we have

$$\frac{u_{i,j,k}^{n+1} - u_{i,j,k}^n}{\Delta t} \Delta x \Delta y \Delta z = \left[ \left( \frac{u_{i+1,j,k}^n - u_{i,j,k}^n}{\Delta x} - \frac{u_{i,j,k}^n - u_{i-1,j,k}^n}{\Delta x} \right) \Delta y \Delta z + \left( \frac{u_{i,j+1,k}^n - u_{i,j,k}^n}{\Delta y} - \frac{u_{i,j,k}^n - u_{i,j-1,k}^n}{\Delta y} \right) \Delta x \Delta z + \left( \frac{u_{i,j,k+1}^n - u_{i,j,k}^n}{\Delta z} - \frac{u_{i,j,k}^n - u_{i,j,k-1}^n}{\Delta z} \right) \Delta x \Delta y \right] \quad (9)$$

where  $n$  is the current time index and  $\Delta t$  is the step size for time discretization. (9) can be written as

$$u_{i,j,k}^{n+1} = u_{i,j,k}^n + \Delta t \left[ \left( \frac{u_{i+1,j,k}^n - u_{i,j,k}^n}{\Delta x^2} - \frac{u_{i,j,k}^n - u_{i-1,j,k}^n}{\Delta x^2} \right) + \left( \frac{u_{i,j+1,k}^n - u_{i,j,k}^n}{\Delta y^2} - \frac{u_{i,j,k}^n - u_{i,j-1,k}^n}{\Delta y^2} \right) + \left( \frac{u_{i,j,k+1}^n - u_{i,j,k}^n}{\Delta z^2} - \frac{u_{i,j,k}^n - u_{i,j,k-1}^n}{\Delta z^2} \right) \right] \quad (10)$$

For boundary control volumes, backward and forward difference approximations of derivative are used additionally. For the control volume at the bottom left corner, (9) is modified as

$$\frac{u_{i,j,k}^{n+1} - u_{i,j,k}^n}{\Delta t} \Delta x \Delta y \Delta z = \left[ \left( \frac{u_{i+1,j,k}^n - u_{i,j,k}^n}{\Delta x} - \frac{u_{i,j,k}^n - uL(j,k)}{\Delta x / 2} \right) \Delta y \Delta z + \left( \frac{u_{i,j+1,k}^n - u_{i,j,k}^n}{\Delta y} - \frac{u_{i,j,k}^n - uF(i,k)}{\Delta y / 2} \right) \Delta x \Delta z + \left( \frac{u_{i,j,k+1}^n - u_{i,j,k}^n}{\Delta z} - \frac{u_{i,j,k}^n - uB(i,j)}{\Delta z / 2} \right) \Delta x \Delta y \right] \quad (11)$$

or

$$u_{i,j,k}^{n+1} = u_{i,j,k}^n + \Delta t \left[ \left( \frac{u_{i+1,j,k}^n - u_{i,j,k}^n}{\Delta x^2} - 2 \frac{u_{i,j,k}^n - uL(j,k)}{\Delta x^2} \right) + \left( \frac{u_{i,j+1,k}^n - u_{i,j,k}^n}{\Delta y^2} - 2 \frac{u_{i,j,k}^n - uF(i,k)}{\Delta y^2} \right) + \left( \frac{u_{i,j,k+1}^n - u_{i,j,k}^n}{\Delta z^2} - 2 \frac{u_{i,j,k}^n - uB(i,j)}{\Delta z^2} \right) \right] \quad (12)$$

where  $uL$ ,  $uF$  and  $uB$  are the boundary values at the left, front and bottom faces of the cube respectively. The iteration scheme for the remaining boundary control volume can be formulated analogously.

### 3. Stability analysis

In order to find the stability condition for the iteration scheme using Von Neumann method, we replace [7]

$$u_{p,q,r}^n = A e^{i\theta_1 p \Delta x} e^{i\theta_2 q \Delta y} e^{i\theta_3 r \Delta z} e^{\alpha(n\Delta t)} = A e^{i\theta_1 p \Delta x} e^{i\theta_2 q \Delta y} e^{i\theta_3 r \Delta z} \xi^\alpha \quad (13)$$

where  $\xi = e^{n\Delta t}$  is an amplification factor,  $i = \sqrt{-1}$ ,  $A$ ,  $\theta_1$ ,  $\theta_2$ , and  $\theta_3$  are constants. The iteration scheme in (10) is stable if  $|\xi| \leq 1$  [3]. Using (13) in (10) and simplifying, we get

$$\xi = 1 + \frac{e^{i\theta_1\Delta x} - 2 + e^{-i\theta_1\Delta x}}{\Delta x^2} + \frac{e^{i\theta_2\Delta y} - 2 + e^{-i\theta_2\Delta y}}{\Delta y^2} + \frac{e^{i\theta_3\Delta z} - 2 + e^{-i\theta_3\Delta z}}{\Delta z^2} \tag{14}$$

For the worst case,  $\theta_1\Delta x = \theta_2\Delta y = \theta_3\Delta z$  [12]. This gives

$$\xi = 1 - \frac{4\Delta t}{\Delta x^2} - \frac{4\Delta t}{\Delta y^2} - \frac{4\Delta t}{\Delta z^2} \tag{15}$$

The stability condition  $|\xi| \leq 1$  yields

$$\frac{\Delta t}{\Delta x^2} + \frac{\Delta t}{\Delta y^2} + \frac{\Delta t}{\Delta z^2} \leq \frac{1}{2} \tag{16}$$

or

$$\Delta t \leq \frac{1}{2} \left( \frac{1}{\Delta x^2} + \frac{1}{\Delta y^2} + \frac{1}{\Delta z^2} \right)^{-1} \tag{17}$$

If  $\Delta x = \Delta y = \Delta z = h$ , then the iteration scheme in (10) is stable if

$$\Delta t \leq \frac{h^2}{6} \tag{18}$$

#### 4. A test problem and solutions

The equation and the conditions used by [1] are chosen as a test problem for this study. The heat equation considered in [1] was

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2}, \quad 0 < x, y, z < 1 \tag{19}$$

with initial condition

$$u(x, y, z, 0) = \sin\left(\frac{\pi}{3}[x + y + z]\right) + xyz, \quad 0 < x, y, z < 1$$

and boundary conditions

$$u(0, y, z, t) = e^{-\frac{\pi^2 t}{3}} \sin\left(\frac{\pi}{3}[y + z]\right), \quad 0 < y, z < 1, \quad t \geq 0$$

$$u(1, y, z, t) = e^{-\frac{\pi^2 t}{3}} \sin\left(\frac{\pi}{3}[1 + y + z]\right) + yz, \quad 0 < y, z < 1, \quad t \geq 0$$

$$u(x, 0, z, t) = e^{-\frac{\pi^2 t}{3}} \sin\left(\frac{\pi}{3}[x + z]\right), \quad 0 < x, z < 1, \quad t \geq 0$$

$$u(x, 1, z, t) = e^{-\frac{\pi^2 t}{3}} \sin\left(\frac{\pi}{3}[x + 1 + z]\right) + xz, \quad 0 < x, z < 1, \quad t \geq 0$$

$$u(x, y, 0, t) = e^{-\frac{\pi^2 t}{3}} \sin\left(\frac{\pi}{3}[x + y]\right), \quad 0 < x, y < 1, \quad t \geq 0$$

$$u(x, y, 1, t) = e^{-\frac{\pi^2 t}{3}} \sin\left(\frac{\pi}{3}[x + y + 1]\right) + xy, \quad 0 < x, y < 1, \quad t \geq 0$$

The exact solution of the test problem is

$$u(x, y, z, t) = e^{\frac{-\pi^2 t}{3}} \sin\left(\frac{\pi}{3}[x + y + z]\right) + xyz$$

To solve (19) with the given initial and boundary conditions by the numerical method discussed so far,  $32 \times 32 \times 32$  cubic finite volume cells of grid size  $\Delta x = \Delta y = \Delta z = \frac{1}{32}$  are taken. The time step of  $\Delta t = 0.0001$  is chosen based on the stability condition (18). Figure 4 shows the contours plot of the finite volume and exact solutions for  $t = 0.05, 0.25, 0.5, 1$ . The solutions along central line of the cube ( $x = 0.5, y = 0.5, 0 \leq z \leq 1$ ) for these times are also displayed in Figure 5. Since the vertical central line does not include the center of the control volumes in the discretization, the average values of temperature on the neighbouring lines ( $x = 0.484375, y = 0.484375, 0 \leq z \leq 1$ ) and ( $x = 0.515625, y = 0.515625, 0 \leq z \leq 1$ ) are used to calculate the values on the vertical central line. The solutions of heat equation using  $16 \times 16 \times 16$  cells and  $t = 0.5$  along the vertical central is depicted with table of values (Table 1).

Table 1. A Comparison between finite volume and exact solutions at  $t = 0.5$ .

z	FV solution	Exact solution	error
0.0000	0.16680689	0.16680689	0.00000000
0.0313	0.17774781	0.17771164	0.00003617
0.0938	0.19901144	0.19897236	0.00003908
0.1563	0.21952329	0.21948181	0.00004148
0.2188	0.23926275	0.23921932	0.00004343
0.2813	0.25821250	0.25816756	0.00004494
0.3438	0.27635860	0.27631255	0.00004605
0.4063	0.29369054	0.29364376	0.00004678
0.4688	0.31020128	0.31015414	0.00004714
0.5313	0.32588732	0.32584018	0.00004714
0.5938	0.34074864	0.34070186	0.00004678
0.6563	0.35478877	0.35474272	0.00004605
0.7188	0.36801474	0.36796980	0.00004494
0.7813	0.38043707	0.38039364	0.00004343
0.8438	0.39206968	0.39202819	0.00004148
0.9063	0.40292990	0.40289082	0.00003908
0.9688	0.41303834	0.41300217	0.00003617
1.0000	0.41778345	0.41778345	0.00000000

The error of the numerical method is indicated in table. As we can observe from the figures and the table, the final volume solution of three-dimensional heat equation is almost identical with that of the exact solution. To get more accurate solution with the numerical method, small mesh spacing is required. This in turn needs small time step to avoid numerical instability in the computation. The algorithm and the MATLAB code of the numerical method are indicated at the appendix.

## 5. Conclusion

In this study, three-dimensional heat equation is solved in a unit cube using a finite volume based numerical method. A MATLAB code is used perform the computation. The stability of the numerical method is analyzed. The solutions obtained by the numerical method are compared with exact solutions and show an excellent agreement. This indicates that the three-dimensional heat equation is discretised properly, the

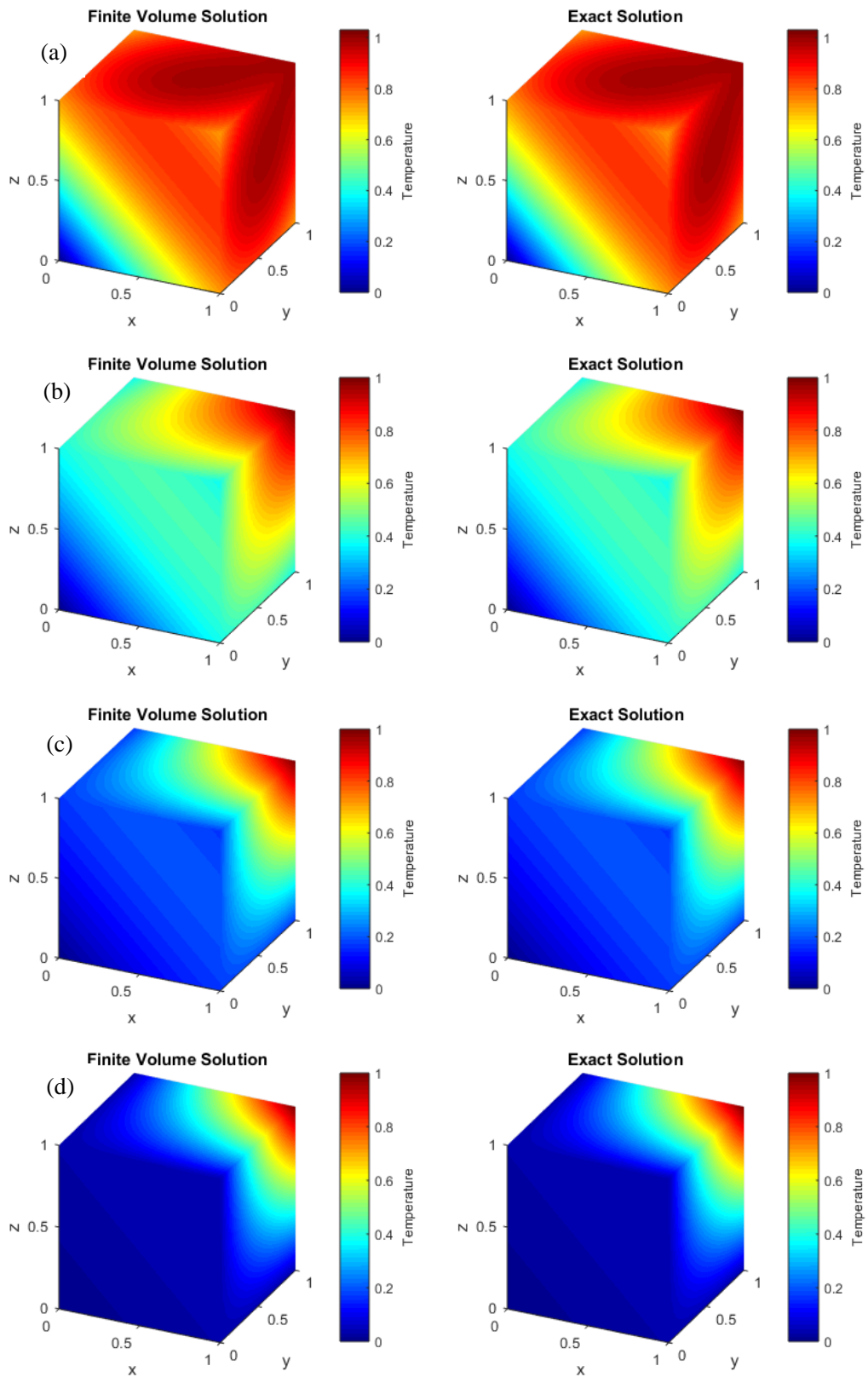


Figure 4. Contour plot of temperature at (a)  $t = 0.05$  (b)  $t = 0.25$  (c)  $t = 0.5$  (d)  $t = 1$ .

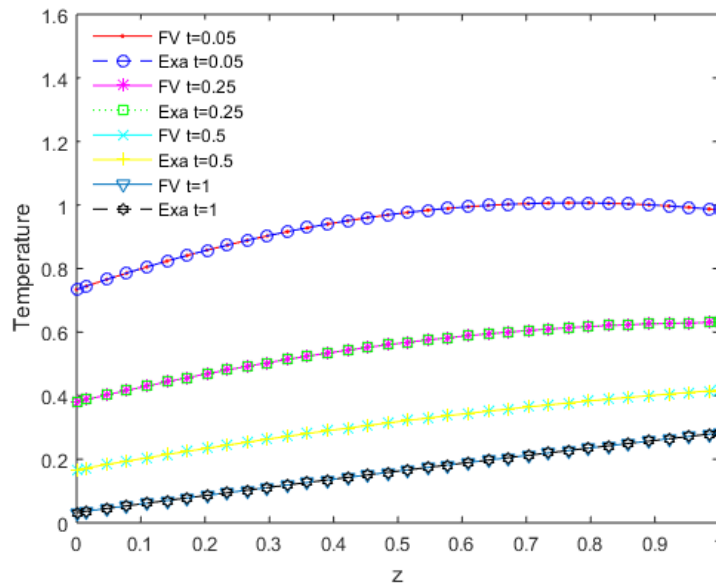


Figure 5. Temperature distribution along the vertical centreline of the cube at different times.

boundary conditions are implemented precisely and the code is written correctly. The findings of this study may provide useful technique to implement a numerical method on a computer in solving partial differential equations in three dimensions.

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## Appendix A: Algorithm for the numerical method

1. Divide the computational domain into uniform Control volumes (cells).
2. Set initial conditions at the center of all control volumes.
3. Impose boundary conditions over the control volume faces at the boundaries of the domain.
4. Compute the temperature at the center of each control volume for the time level using (10), (11), (12) and other related equations.
5. Repeat step 4 for the next time increment until the convergence criteria is satisfied.
6. Use 3D Matrix to represent temperature distribution in the domain.
7. Display the solution result in tabular form or as graphs.

## Appendix B: MATLAB code for the numerical method

```
%heat3d
clear all; close all; clc;
T=1;
dt=0.0001; %Von Neumann stability analysis:For dx=dy=dz=h, take dt<=h^2/6
Nt=T/dt;
t=(1:Nt)*dt;
Nx=32;Ny=32;Nz=32;
dx=1/Nx;dy=1/Ny;dz=1/Nz;
xc=dx/2:dx:(1-dx/2);
yc=dy/2:dy:(1-dy/2);
zc=dz/2:dz:(1-dz/2);
x=[0 xc 1];
y=[0 yc 1];
z=[0 zc 1];
u=zeros(Nx,Ny,Nz);
u2=zeros(Nx,Ny,Nz);
%Initial condition
tic
for k=1:Nz
    for j=1:Ny
        for i=1:Nx
            u(i,j,k)=sin((pi/3)*(xc(i)+yc(j)+zc(k)))+xc(i)*yc(j)*zc(k);
        end
    end
end
for K=1:Nt
    for k=1:Nz
        for j=1:Ny
            for i=1:Nx
                %Boundary Conditions at the faces
                uB(i,j)=exp(-pi^2*t(K)/3).*sin((pi/3)*(xc(i)+yc(j))); %bottom face
                uT(i,j)=exp(-pi^2*t(K)/3).*sin((pi/3)*(xc(i)+yc(j)+1))+xc(i).*yc(j); %top face
                uF(i,k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(xc(i)+zc(k))); %front face
                uBC(i,k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(xc(i)+zc(k)+1))+xc(i).*zc(k); %back face
                uL(j,k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(yc(j)+zc(k))); %left face
                uR(j,k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(yc(j)+zc(k)+1))+yc(j).*zc(k); %right face
                %Boundary conditions at the edges
                uLBE(j)=exp(-pi^2*t(K)/3).*sin((pi/3)*(0+yc(j))); %left bottom edge
                uRBE(j)=exp(-pi^2*t(K)/3).*sin((pi/3)*(1+yc(j))); %right bottom edge
                uLTE(j)=exp(-pi^2*t(K)/3).*sin((pi/3)*(0+yc(j)+1)); %left top edge
                uRTE(j)=exp(-pi^2*t(K)/3).*sin((pi/3)*(1+yc(j)+1))+yc(j); %right top edge
                uFLE(k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(0+zc(k))); %Front left edge
                uFRE(k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(1+zc(k))); %Front right edge
                uLBCE(k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(1+zc(k))); %left back edge
                uRBCE(k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(1+zc(k)+1))+zc(k); %Right back edge
            end
        end
    end
end
% Boundary conditions at the edges
for k=1:Nz+2
    for j=1:Ny+2
```

```

for i=1:Nx+2
uFBE(i)=exp(-pi^2*t(K)/3).*sin((pi/3)*(x(i)+0)); %Front bottom edge
uBCBE(i)=exp(-pi^2*t(K)/3).*sin((pi/3)*(x(i)+1)); %back bottom edge
uFTE(i)=exp(-pi^2*t(K)/3).*sin((pi/3)*(x(i)+0+1)); %Front top edge
uBCTE(i)=exp(-pi^2*t(K)/3).*sin((pi/3)*(x(i)+1+1))+x(i);%Back top edge
end
end
end
for k=1:Nz
for j=1:Ny
for i=1:Nx
if i==1
if j==1
if k==1
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+(u(i,j+1,k)-u(i,j,k))/(dy^2)-2*(u(i,j,k)-uF(i,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-2*(u(i,j,k)-uB(i,j))/(dz^2))+u(i,j,k);
elseif k==Nz
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+(u(i,j+1,k)-u(i,j,k))/(dy^2)-2*(u(i,j,k)-uF(i,k))/(dy^2)...
+2*(uT(i,j)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
else
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+(u(i,j+1,k)-u(i,j,k))/(dy^2)-2*(u(i,j,k)-uF(i,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
end
elseif j==Ny
if k==1
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-2*(u(i,j,k)-uB(i,j))/(dz^2))+u(i,j,k);
elseif k==Nz
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+2*(uT(i,j)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
else
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
end
else
if k==1
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+(u(i,j+1,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-2*(u(i,j,k)-uB(i,j))/(dz^2))+u(i,j,k);
elseif k==Nz
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+(u(i,j+1,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+2*(uT(i,j)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
else
u2(i,j,k)=dt*((u(i+1,j,k)-u(i,j,k))/(dx^2)-2*(u(i,j,k)-uL(j,k))/(dx^2)...
+(u(i,j+1,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
end
end
elseif i==Nx
if j==1
if k==1
u2(i,j,k)=dt*(2*(uR(j,k)-u(i,j,k))/(dx^2)-(u(i,j,k)-u(i-1,j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-2*(u(i,j,k)-uF(i,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-2*(u(i,j,k)-uB(i,j))/(dz^2))+u(i,j,k);
elseif k==Nz
u2(i,j,k)=dt*(2*(uR(j,k)-u(i,j,k))/(dx^2)-(u(i,j,k)-u(i-1,j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-2*(u(i,j,k)-uF(i,k))/(dy^2)...
+2*(uT(i,j)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
else
u2(i,j,k)=dt*(2*(uR(j,k)-u(i,j,k))/(dx^2)-(u(i,j,k)-u(i-1,j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
end
end
elseif j==Ny
if k==1
u2(i,j,k)=dt*(2*(uR(j,k)-u(i,j,k))/(dx^2)-(u(i,j,k)-u(i-1,j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-2*(u(i,j,k)-uB(i,j))/(dz^2))+u(i,j,k);
elseif k==Nz
u2(i,j,k)=dt*(2*(uR(j,k)-u(i,j,k))/(dx^2)-(u(i,j,k)-u(i-1,j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+2*(uT(i,j)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
else
u2(i,j,k)=dt*(2*(uR(j,k)-u(i,j,k))/(dx^2)-(u(i,j,k)-u(i-1,j,k))/(dx^2)...
+2*(uBC(i,k)-u(i,j,k))/(dy^2)-(u(i,j,k)-u(i,j-1,k))/(dy^2)...
+(u(i,j,k+1)-u(i,j,k))/(dz^2)-(u(i,j,k)-u(i,j,k-1))/(dz^2))+u(i,j,k);
end
end
else
if k==1

```



```

for k=1:Nz+2
    for j=1:Ny+2
        for i=1:Nx+2

uexa(i,j,k)=exp(-pi^2*t(K)/3).*sin((pi/3)*(x(i)+y(j)+z(k)))+x(i)*y(j)*z(k);
            end
        end
    end
end
toc
% U
% uexa
[Xc,Yc,Zc]=meshgrid(xc,yc,zc);
%slice(X,Y,Z,u2,xc,yc,zc)
[X,Y,Z]=meshgrid(x,y,z);
% figure % Finite volume solution
subplot(1,2,1)
slice(X,Y,Z,U,x,y,z);
xlabel('x');
ylabel('y');
zlabel('z')
view(25,26)
colormap(jet)
cb=colorbar;
cb.Label.String='Temperature';
title('Finite Volume Solution')
shading interp
% figure %Exact solution
subplot(1,2,2)
slice(X,Y,Z,uexa,x,y,z);
xlabel('x');
ylabel('y');
zlabel('z')
view(25,26)
colormap(jet)
cb=colorbar;
cb.Label.String='Temperature';
title('Exact Solution')
shading interp
figure % Along the vertical central line
uxmid=(U(:,(Ny/2)+1,(Nz/2)+1)+U(:,(Ny/2)+2,(Nz/2)+2))/2;
uzmid=(U((Nx/2)+1,(Ny/2)+1,:)+U((Nx/2)+2,(Ny/2)+2,:))/2;
uexaxmid=(uexa(:,(Ny/2)+1,(Nz/2)+1)+uexa(:,(Ny/2)+2,(Nz/2)+2))/2;
uexazmid=(uexa((Nx/2)+1,(Ny/2)+1,:)+uexa((Nx/2)+2,(Ny/2)+2,:))/2;
for k=1:Nz+2;
    uzmid1(k)=uzmid(k);
    uexazmid1(k)=uexazmid(k);
end
err=abs(uexazmid1-uzmid1);
plot(z,uzmid1,'r.-',z,uexazmid1,'bo-');
legend('FV solution','Exact solution','Location','NorthWest');
xlabel('z')
ylabel('Temperature')
% Table of values
fprintf(' z      FV solution      Exact solution      error\n')
for k=1:Nz+2
    fprintf('%2.5f      %2.8f      %2.8f      %2.8f \n',z(k),uzmid1(k),uexazmid1(k),err(k))
end

```